

CLAIMS

1. A gas phase olefin polymerization process comprising:

- (1) preparing a solution of a catalyst precursor comprising a mixture of magnesium and titanium compounds, an electron donor and a solvent;
- 5 (2) adding a filler to the solution from step (1) to form a slurry;
- (3) spray drying the slurry from step (2) at a temperature of 100 to 140°C to form a spray dried precursor;
- (4) slurrying the spray dried precursor from step (3) in mineral oil,
- (5) partially or fully pre-activating the catalyst precursor by contacting the slurry of (4)
- 10 with one or more Lewis Acids, and
- (6) transferring the partially or fully activated precursor from step (5) into a gas phase reactor in which an olefin polymerization reaction is in progress.

2. A gas phase olefin polymerization process comprising:

- (1) preparing a solution of a catalyst precursor comprising a mixture of magnesium
- 15 and titanium compounds, an electron donor and a solvent;
- (2) adding a porous catalyst support, to the solution from step (1) to form a slurry;
- (3) drying the slurry from step (2) to form a solid catalyst precursor;
- (4) slurrying the solid precursor from step (3) in a viscous inert liquid,
- (5) partially or fully pre-activating the catalyst precursor by contacting the slurry of
- 20 (4) with one or more Lewis Acids, and
- (6) transferring the partially or fully activated precursor from step (5) into a gas phase reactor in which an olefin polymerization reaction is in progress.

3. The process of Claim 1 or 2 wherein;

- 1) the catalyst precursor in step (1) corresponds to the formula:



wherein R is an aliphatic or aromatic hydrocarbon radical having 1 to 14 carbon atoms or COR' wherein R' is a aliphatic or aromatic hydrocarbon radical having 1 to 14 carbon atoms and each OR group is the same or different;

M is a transition metal;

30 X is independently chlorine, bromine or iodine;

ED is an electron donor;

d is 0.5 to 56; e is 0, 1, or 2; f is 2 to 116; g is >2 and up to 1.5(d) + 3; and

2) the Lewis Acid of step (5) is

- i) one or more compounds with formula  $\text{M}'(\text{R}'')_n\text{X}_{(3-n)}$  wherein M' is aluminum or
- 35 boron; each X is independently chlorine, bromine, or iodine; each R'' is independently a saturated aliphatic hydrocarbon radical having 1 to 14 carbon atoms, provided that when M is aluminum, n is 1 to 3 and when M is boron, n is 0 to 1.5; and

ii) is added in an amount such that the mole ratio of total Lewis Acid to electron donor in the precursor is from 0.10:1 to 1.0:1.

4. The process of Claim 1 or 2, wherein said Lewis Acid is;

1) one or more alkylaluminum compound(s) with formula  $M'(R'')_nX_{(3-n)}$  wherein  $M'$  is aluminum,  $R''$  is n-butyl, n-hexyl, n-octyl, iso-octyl, isohexyl, and n-decyl, X is Cl or Br and n is a number from 0 to 1.5; and

2) added in an amount such that the mole ratio of total Lewis Acid to electron donor in the precursor is from 0.10:1 to 0.75:1.

5. The process of Claim 4, wherein said Lewis Acid is;

1) selected from the group consisting triethylaluminum, tri-n-butyl aluminum, tri-n-hexyl aluminum, tri-n-octyl aluminum, tri n-decyl aluminum, triisoprenyl aluminum, dimethyl aluminum chloride, ethylaluminum dichloride, diethylaluminum chloride, and mixtures thereof; and

2) added in an amount such that the mole ratio of total Lewis Acid to electron donor in the precursor is from 0.10:1 to 0.30:1.

6. The process of Claim 4 wherein said Lewis Acid is a sequential mixture of tri-n-hexylaluminum and diethylaluminum chloride; a sequential mixture of triethylaluminum and diethylaluminum chloride; a sequential mixture of diethylaluminum chloride and tri-n-hexylaluminum; or a sequential mixture of diethylaluminum chloride and triethylaluminum.

7. The process of Claim 1 or 2 wherein the amount of polymer fines produced in said gas phase polymerization is at least 10 percent less than the amount produced in an analogous process but without the pre-activation of step (5).

8. The process of Claim 1 or 2 in which the slurry of (2) is intimately mixed with the Lewis Acid by use of a static mixer.

9. The process of Claim 1 or 2 in which said a gas phase reactor is in a single reactor configuration.

10. The process of Claim 1 or 2 in which said a gas phase reactor in which an olefin polymerization reaction is in progress is the first reactor in a multiple series reactor configuration.

11. The process of Claim 10 wherein said multiple series reactor configuration is a dual series reactor configuration.